

$XE_{b\ kir}^p ; XE_{b\ chiq}^p$ - X energy of low-potential heat carrier (water) in the inlet and outlet areas of the evaporator, respectively, kJ / kg.

$XE_{k\ kir}^{yu} ; XE_{k\ chiq}^{yu}$ - Exergy X energy of high-potential cooling water in the inlet and outlet areas of the condenser, respectively, kJ / kg.

$XE_{kon\ kir}^{XA} ; XE_{k\ chiq}^{XA}$ - X energy of the coolant (chlodagen) in the inlet and outlet areas of the condenser, kJ / kg.

$XE_{kom\ kir}^{XA} ; XE_{kom\ chiq}^{XA}$ - X energy of the coolant in the inlet and outlet areas of the compressor, kJ / kg.

$XE_{dr\ kir}^{XA} ; XE_{dr\ chiq}^{XA}$ - X energy of the coolant in the inlet and outlet areas of the throttle, kJ / kg.

$\Delta XE_b'$ - X energy loss in the evaporator, kJ / kg.

$\Delta XE_{kom\ ish}'$ - loss of X energy in the compressor under the influence of friction, kJ / kg.

$\Delta XE_{kom\ in}'$ - X energy loss in the compressor, kJ / kg.

$\Delta XE_{kon}'$ - X energy loss in the capacitor, kJ / kg.

$\Delta XE_{dr}'$ - X energy loss in the throttle, kJ / kg.

The total thermal X energy of a low and high potential heat carrier (water) is expressed as follows:

$$XE_i = G_i \cdot e_i \quad (1.1)$$

Where G_i - heat transfer fluid consumption, kg / s;

e_i - specific X energy of the liquid flow at the appropriate temperature, kJ / kg

The specific X energy of the fluid flow, kJ / kg, is determined as follows.

$$e_i = \tau_i \cdot h_i$$

where τ_i - the thermodynamic function of the cooling water flow, determined by the formula

$$\tau_i = 1 - \frac{(273 + t_{t.m})}{T_i}$$

Here, $t_{t.m}$ the temperature of the external environment °C;

T_i - temperature of the liquid at a certain point °C;

h_i - enthalpy of the medium at a given point, kJ / kg.

The X energy of a low-potential heat carrier (water) is as follows.

$$XE_{b\ kir}^p = G_p \cdot e_{b\ kir}^p = \tau_{b\ kir}^p \cdot h_4 \quad (1.2)$$

Here, h_4 - enthalpy of xlodgen before evaporator, kJ / kg;

$\tau_{b\ kir}^p$ - Thermodynamic function of low-potential chlodge at the entrance to the evaporator.

$$\tau_{b\ kir}^p = 1 - \frac{(273+t_{t.m})}{T_{b\ kir}^p}, \quad (1.3)$$

$T_{b\ kir}^p$ - temperature at which the low- potential xlodge enters the evaporator, K

$$\text{Conclusion } XE_{b\ chiq}^p = G_p \cdot e_{b\ chiq}^p = \tau_{b\ chiq}^p \cdot h_1 ; \quad (1.4)$$

$$\tau_{b\ chiq}^p = 1 - \frac{(273+t_{t.m})}{T_{b\ chiq}^p} ; \quad (1.5)$$

Here h_1 is the enthalpy of chlodge after evaporation, kJ / kg;

$T_{b\ chiq}^p$ - evaporator temperature of low-potential chlodge, K

Similarly, the X energy of a high-potential heat carrier is as follows.

$$XE_{k\ kir}^{yu} = G_{yu} \cdot e_{k\ kir}^{yu} = \tau_{k\ kir}^{yu} \cdot h_{2a} \quad (1.6)$$

Here, h_{2a} is the enthalpy of xlodgen before the evaporator, kJ / kg, where the thermodynamic function of the low-potential coolant entering the condenser is as follows.

$$\tau_{k\ kir}^{yu} = 1 - \frac{(273+t_{t.m})}{T_{k\ kir}^{yu}}; \quad (1.7)$$

Here $T_{k\ kir}^{yu}$ is the temperature at which the high-potential chlodge exits the heat pump heating system, K.

The thermodynamic function of the X energy of the chlodge before and after the compressor is expressed as follows.

$$XE_{kom\ kir}^{XA} = G_{XA} \cdot e_{kom\ kir}^{XA} = \tau_{kom\ kir}^{XA} \cdot h_1; \quad (1.8)$$

$$\tau_{kom\ kir}^{XA} = 1 - \frac{(273+t_{t.m})}{273+t_1}; \quad (1.9)$$

$$XE_{kom\ chiq}^{XA} = G_{XA} \cdot e_{kom\ chiq}^{XA} = \tau_{kom\ chiq}^{XA} \cdot h_{2a}; \quad (1.10)$$

$$\tau_{kom\ chiq}^{XA} = 1 - \frac{(273+t_{t.m})}{273+t_{2a}}; \quad (1.11)$$

The energy of chlodge for the remaining areas of the heat pump heating system, for the condenser

$$XE_{kon\ kir}^{XA} = XE_{kom\ chiq}^{XA}; \quad (1.12)$$

$$XE_{kon\ chiq}^{XA} = G_{XA} \cdot e_{kon\ chiq}^{XA} = \tau_{kon\ chiq}^{XA} \cdot h_3; \quad (1.13)$$

$$\tau_{kon\ chiq}^{XA} = 1 - \frac{(273+t_{t.m})}{273+t_3}; \quad (1.14)$$

for the throttle

$$XE_{kom\ chiq}^{XA} = XE_{dr\ kir}^{XA}; \quad (1.15)$$

$$XE_{dr\ chiq}^{XA} = G_{XA} \cdot e_{dr\ chiq}^{XA} = \tau_{dr\ chiq}^{XA} \cdot h_4; \quad (1.16)$$

$$\tau_{dr\ chiq}^{XA} = 1 - \frac{(273+t_{t.m})}{273+t_4}; \quad (1.17)$$

To develop a mathematical model of X energy flows, it is necessary to define the concepts of “product X energy” and “heat X energy”. “Product exergy” includes X energy produced by a high-potential heat carrier in a condenser and an intermediate heat exchanger. the “heat X energy” consists of the water vapor in the evaporator, the X energy given for the cycle in the heat pump heating system, and the X energy given to the refrigerant during the compression process.

The total X energy of a heat pump heating system using a heat carrier is as follows

$$(XE_{b\ kir}^p - XE_{b\ chiq}^p + XE_{b\ kir}^{XA} - XE_{b\ chiq}^{XA} - \Delta XE'_b) + (XE_{kom\ kir}^{XA} - XE_{kom\ chiq}^{XA} + \Delta XE'_{kom\ ish} - \Delta XE'_{kom\ in}) + (XE_{kon\ kir}^{XA} - XE_{kon\ chiq}^{XA} + XE_{kon\ kir}^{yu} - XE_{kon\ chiq}^{yu} - \Delta XE'_{kon}) + (XE_{dr\ kir}^{XA} - XE_{dr\ chiq}^{XA} - \Delta XE'_{dr}) + E_{nas} = 0; \quad (1.18)$$

“Product “Product Exergy” is equivalent to the following;

$$XE_{b\ kir}^p + XE_{kon\ kir}^{yu} + \Delta XE'_{kom\ ish} + E_{nas} = XE_{b\ chiq}^p + XE_{kon\ chiq}^{yu} + \Delta XE'_b + \Delta XE'_{kom\ in} + \Delta XE'_{dr}; \quad (1.19)$$

Here E_{nas} X of the pump power

$$E_{nas} = N_{ss} + N_{is} + N_{ch}; \quad (1.20)$$

Here the N_{ss}, N_{it}, N_{ch} power of the pump to actuate the high-potential coolant, heat-carrying fluid, and liquid waste storage tank waste, V_t .

The X energy loss in the sections of a heat pump heating system can be expressed by the following equation.

$$\Delta X E'_b = \tau_b^p (h_1 - h_4) - [(h_1 - h_4) - (273 + t_{t.m})(t_4 - t_1)]; \quad (1.21)$$

$$\Delta X E'_{kon} = (h_{2a} - h_3) - (273 + t_{t.m})(t_{2a} - t_3) - \tau_b^p (h_{2a} - h_3); \quad (1.22)$$

$$\Delta X E'_{dr} = (273 + t_{t.m})(t_4 - t_3); \quad (1.23)$$

$$\Delta X E'_{kom\ ish} = \frac{(h_{2a} - h_1)}{\eta_{kom} \cdot \eta_{ed}} - (h_{2a} - h_1); \quad (1.24)$$

$$\Delta X E'_{kom\ in} = (273 + t_{t.m})(t_{2a} - t_1); \quad (1.25)$$

Here η_{kom}, η_{ed} is the efficiency of the compressor and its electric motor.

The X energy of the cooling water at each individual point is determined taking into account the ambient temperature, so the limit values are determined in the calculation. The advantage of X energy balance is that it takes into account the effect of heat.

In this case, the "heat X energy" is as follows

$$E'_{is} = \Delta X E'_{kom\ ish} + E_{nas}; \quad (1.26)$$

The efficiency of X is equal to

$$\eta_{Xe} = \frac{X E'_b\ chiq + X E'_{k\ chiq}}{\Delta X E'_{kom\ ish} + E_{nas}}; \quad (1.27)$$

The resulting X energy model allows the detection and analysis of energy flows of a heat pump heating system, as well as the detection of energy effects in the system.

Reference

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